Estimation of Grinding Time for Desired Particle Size Distribution and for Hematite Liberation Based on Ore Retention Time in the Mill



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Received: 27 August 2019 / Accepted: 16 December 2019 / Published online: 3 January 2020 © Society for Mining, Metallurgy & Exploration Inc. 2020

Abstract

Iron ores obtained from different sources differ in their chemical and physical properties. These variations make the process of grinding a difficult task. The work carried out in this context focuses on three different samples of iron ore, viz., high silica high alumina, low silica high alumina, and low silica low alumina. The grinding process for all the three iron ores is carried out individually in Bond's ball mill and the total retention time taken by each iron ore sample is calculated. The present investigation focuses on utilizing the calculated retention time of the iron ore as a standard grinding reference time to the laboratory ball mill for optimizing the grinding time of each ore. The desired P_{80} (150 µm) with an acceptable range of hematite liberation (>75%) was obtained in the laboratory ball mill after reducing 6 min from the total retention time taken in the Bond ball mill.

Keywords Particle size distribution (PSD) · Retention time · Comminution · Characterization studies

1 Introduction

Ball mills are progressively used to grind the ores for particle size reduction and to liberate valuable minerals from the ores. The grinding of ore is a highly energyintensive process [1-4]. In this process, the size of the particle obtained depends on the energy consumption of the ball mill. The major challenge encountered in the process of iron ore grinding is to maintain the desired product particle size distribution (PSD) with sufficient liberation of valuable minerals. The demand for desired particle size with maximum liberation of valuables is increasing, particularly in the last phase of the grinding, for primary feed preparation for the making of pellets.

There are many tests for determining grindability. The most commonly used test is the Bond ball mill (BBM). It enables the installation of a plant scale ball mill [5]. The Bond work

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index test is used to measure the energy required for the desired particle size reduction and for designing new circuits for comminution [5]. The Bond work index is commonly agreed as a grindability factor for ores in order to relate different material compositions [6]. Several works related to the strength of the Bond test with respect to the grindability factor are discussed [7–13].

The Bond test analysis specifies that one of the vital parameters for computing work indices is PSD [9]. In this sense, the standard Bond test procedure is used to analyze PSD in terms of F_{80} and P_{80} parameters.

It is well-recognized in conventional grinding that PSD and effective liberation of valuable materials from the gangue, which occurs at different particle sizes, depends mainly on the properties of the ore being ground. The liberation properties of the valuables depend on its chemical and physical composition, which helps in the selection of the processing methods enabling effective utilization of the iron ore [14–17]. The size reduction and liberation of the particles are accomplished by the grinding process [18]. It is often hard to control the PSD in the end product. In a combined mineral processing, the liberation of valuables assists as a link between the grinding and the separation by creating particle structure information for the ground products [19]. However, it has been documented that there is an

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uneven breakage in ores, which leads to uneven liberation of minerals [20, 21].

The production of the desired PSD for different source of ores is difficult whenever a ball mill operates at constant operating parameters [18]. The variation in PSD might be due to the different trends in the mineralogical and physical composition of a representative sample from various sources [22]. The mineralogical characterization is considered as a vital tool governing the process of grinding and liberation-related productivity improvement. The study of microstructure and mineralogy plays a significant role in understanding mineral behavior at different stages of the grinding process [23].

In the present scenario, characterization studies were being carried out pertaining to ore liberation and associations of mineral phases, grain size, and textural features by using automated microscopic techniques [24–26]. Improvement of computerized microscopic systems has now made it possible to scan the mineral components of different types of ores [27]. An ore can be characterized by QEMSCAN based on the presence of minerals and their association with respect to every single mineral [28, 29]. The analysis rate of QEMSCAN is rapid to determine the mineralogy and individual ore particle size measurement. The QEMSCAN analysis data consists of mineral association, the grain size of the minerals, and the phase of the minerals.

Along with different operating parameters of the mill and mineralogical characterization, the residence time distribution (RTD) of the mill also plays a very important role in the design of the ball mill circuit. Numerous studies have focused on RTD measurement with respect to solid flow effect, solid transport alongside the mill axis, and variation of ball mill diameter on RTD in the ball mill [30–32]. The different types of RTD measurement methods used were attainable region technique, one-parameter RTD model, and radioactive tracer [33–35].

However, from the literature survey, it was observed that PSD and size-by-size liberation in the fine grinding phase are not clear with a variation of grinding time [36–39]. Hence, the liberation of minerals from ores is still uncertain and conflicting, and this may be associated with the mineralogical textures of dissimilar ores. Furthermore, the difference in the relation between PSD and hematite liberation in the product size has not been specified clearly in earlier works.

The aim of the present study is to measure the total retention time of high silica high alumina (HSHA), low silica high alumina (LSHA), and low silica low alumina (LSLA) iron ore samples using a new approach. Also, the measured total retention time of each ore as a standard reference grinding time was used to achieve the desired P_{80} passing percentage of 150 µm with an acceptable range of hematite liberation (> 75%) from iron ores for the pellet making process by using BBM and laboratory ball mill (LBM).

2 Experimental Method

2.1 Samples

In the present study, iron ore of three different chemical compositions was selected from Karnataka region. These samples are typical raw materials used in JSW Steel, Ballari Pellet Plant, to produce pellets. The selected iron ores are mainly classified into three groups based on the percentage of silica and alumina present in each sample, as shown in Table 1. The chemical composition of the selected iron ore samples is shown in Table 2. In the crushing machine, all the three iron ore samples were crushed to -3 mm and analyzed for the desired P_{80} passing (-150 µm) and percentage of hematite liberated in the three feed iron ore samples. The - 150-µm feed size fractions were selected to determine the nominal degree of hematite liberation from the representative HSHA, LSHA, and LSLA feed iron ore samples. The crushed - 3-mm iron ore samples were used as feed to the BBM and LBM. The processing flow sheet is represented in Fig. 1.

2.2 Grinding Studies

Two kinds of mills, BBM and LBM, were used to achieve the desired P_{80} passing percentage of 150 µm with an acceptable range of hematite liberation (> 75%) at optimum grinding time. The BBM is a standard ball mill having a length and diameter of 300 mm × 300 mm with smooth liner as shown in Fig. 2. A rotating drum is attached to a gearbox and has adjustable speed knob. The number of steel balls and the weight of the balls are selected according to Bond's standard procedure [40].

A bench test was developed for dry grinding to determine the Bond work index and to know the PSD and hematite liberation in all the three iron ore product samples obtained from the BBM. For each iron ore sample, 700 cc of feed was weighed and added into the BBM. The BBM was set for 100 revolutions in the first iteration. The product from the mill was withdrawn after completion of 100 revolutions. The product was then screened and analyzed. Oversized fractions were added back into the mill (as it is a closed-circuit operation). The amount of fresh feed added to the mill is equal to the amount of undersized fractions produced in the first iteration. The number of revolutions for the second iteration is determined based on Bond's standard test procedure [40]. The experiments were continued for a minimum of five consecutive iterations until the net grams per revolution became constant.

A new method was adopted to measure the total retention time taken by each ore in the BBM. The
 Table 1
 Percentage variation of silica and alumina by weight in iron ore

Sl. no.	Type of ore	Silica% by wt. in iron ore	Alumina% by wt. in iron ore
1	HSHA iron ore	>4.5	> 3.5
2	LSHA iron ore	< 4.5	> 3.5
3	LSLA iron ore	<4.5	< 3.5

retention time of the ore in the mill is measured based on the total number of revolutions taken by each ore to produce 250% of circulating load. The number of revolutions for each trail is set to the BBM based on Bond's procedure. For each trial, the set number of revolutions is recorded and represented as R_1 , R_2 , R_3 , R_4 , R_n . The total number of revolutions taken by each ore sample in the BBM is calculated using Eq. 1.

$$\mathbf{R} = \mathbf{R}_1 + \mathbf{R}_2 + \mathbf{R}_3 + \mathbf{R}_4 + \dots + \mathbf{R}_{n-1} + \mathbf{R}_n \tag{1}$$

The total retention time taken by the BBM for each iron ore sample is given by Eq. (1).

T =	Total number of revolution taken by BBM to produce 250% circulating load for each iron ore sample
	number of revolutions per minute

The standard equation used to determine the work index is given in Eq (3).

$$BWI = \frac{48.95}{A^{0.23} \times G_{bp}^{0.82} \left(\frac{10}{\sqrt{P_{80}}} - \frac{10}{\sqrt{F_{80}}}\right)} kWh/t$$
(3)

where F_{80} is 80% passing particle size of the feed in μ m, P_{80} is 80% passing particle size of the final grinding cycle product in μ m, A is the mesh size of the test in m, and G_{bp} is the grindability of the undersized product produced per mill revolution (g/rev).

The same feed samples of HSHA, LSHA, and LSLA used in the BBM are used as feed for the LBM. The test mill has an internal diameter of 500 mm, and it is 1000 mm long as shown in Fig. 3. In the LBM, the experiments were conducted based on the total retention time taken by HSHA, LSHA, and LSLA iron ore samples in the BBM. The LBM experiments were performed based on trial and error method, i.e., by reducing the total retention time obtained from BBM by 2 min, 4 min, and 6 min for the HSHA, LSHA, and LSLA samples, respectively.

For all the samples, the speed of the mill, feed to the mill, and media (balls) were kept constant. The only parameter, which

 Table 2
 Chemical composition of iron ores

Sl. no.	Type of ore	Fe%	SiO ₂ %	$Al_2O_3\%$	LOI%
1	HSHA iron ore	60.42	5.58	4.03	3.17
2	LSHA iron ore	59.51	3.21	4.71	5.09
3	LSLA iron ore	61.09	3.36	2.76	4.36

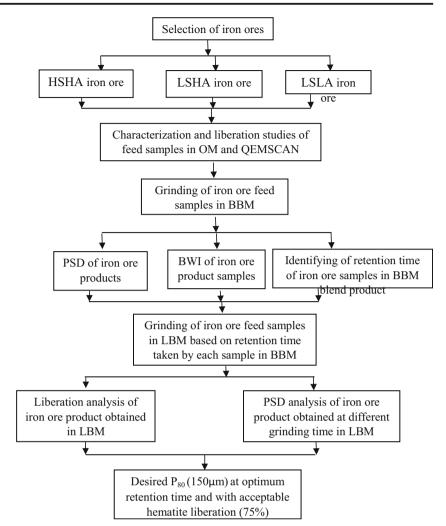
varied in the LBM, was the grinding time. The grinding time of LBM in each case was changed by reducing 2 min from the total retention time taken to produce 250% circulating load in the BBM. After the completion of each experiment in the LBM, particle size analysis was carried out to identify the P_{80} passing percentage particle size fraction and percentage of liberation. The operations were repeated in the LBM for the HSHA, LSHA, and LSLA samples until the P_{80} passing particle size fraction of 150 µm was achieved.

2.3 Techniques Used

Sieve analysis was carried out with the help of a Ro-Tap reciprocating mechanical sieve shaker to determine the percentage of the different grain sizes contained in the samples. The particle size analysis of the three iron ore feed samples is given in Fig. 4. It was observed from the feed analysis that 80% passing of the particles is of sizes below 2.5 mm, 2.4 mm, and 2.7 mm for the HSHA, LSHA, and LSLA iron ore samples, respectively. The density of all the three feed samples was determined using the Pycnometer. The particle density of the three feed samples varied from one another. The particle density of the feed sample was found to be 3.36 g/cm^3 , 3.47 g/cm³, and 3.52 g/cm³ in HSHA, LSHA, and LSLA, respectively. The sink and float study was carried out to analyze the percentage of liberation of hematite in the grounded ore sample using organic liquid with a density of 3.3 g/cm^3 (diiodomethane). About $-150 \,\mu m$ size fractions were selected to determine the nominal degree of liberation of the representative HSHA, LSHA, and LSLA iron ore samples.

(2)

Fig. 1 Process flow sheet to achieve the desired P_{80} (150 µm) at optimum retention time and with acceptable hematite liberation



The micrographs and degree of hematite liberation from the iron ore feed samples were analyzed and compared using the optical microscope (model Leica DMLP) and the QEMSCAN (Quanta FEG 650).

For the liberation study, -150-µm particles were screened from the feed and product samples. For both the feed and product samples, polished specimens were prepared and analyzed in an optical microscope. The volumetric grade in the valuable minerals is statistically equivalent to the surface concentration and is expressed as given in Eq. 4.

$$T\% = \frac{Total area of valuable minerals}{Total area of particles} *100$$
(4)

The following Eq 5. ratio expresses the apparent degree of liberation of the sample of particles represented in a section of the sample.

$$L\% = \frac{Total \ are \ of \ valuable \ minerals}{Total \ are \ of \ mineralized \ particles} *100$$
(5)

3 Results and Discussion

3.1 Mineralogical Analysis of Feed Sample by Optical Microscopy and QEMSCAN

Figure 5 a, b, and c illustrate the mineralogical analysis of the feed samples of HSHA, LSHA, and LSLA using an optical microscope. The analysis derived through optical microscopy was measured with a discontinuous method. Figure 5 a and b represent HSHA and LSHA samples with a significant portion of hematite and are majorly distributed in spheroid form. In addition to this, some finer tubular structures of hematite are also observed in the optical microscopy. However, a major portion of HSHA is composed of Fe Ox-Al silicate interphase and goethite. The LSLA sample consists of major portions of hematite, and it is well-distributed in tubular and spheroid form, whereas LSHA samples include a minor part of limonite and kaolinite as shown in Fig. 5c. The gangue minerals in both LSHA and HSHA are majorly distributed in guartz form and other gangue minerals such as kaolinite and alumina are distributed separately from the quartz.



Fig. 2 Bond's ball mill

Figure 6 a, b, and c show the mineralogical analysis of the feed samples of HSHA, LSHA, and LSLA using the QEMSCAN Quanta FEG 650. The report obtained from the QEMSCAN was three major selections of field image, bulk mineral analysis (BMA), and particle mineral analysis (PMA). In the samples, HSHA and LSHA of Fig. 6 a and b, respectively, the major quantified phase is hematite. From Fig. 6c, in the LSLA sample, most of the quartz is present in the bulk phase, which can be liberated easily by controlled grinding. In the samples of HSHA and LSHA, the quartz phase has a high proportion of hematite in composite form, and hence, the removal of gangue material from the hematite will require intensive grinding.

3.2 Grinding and Liberation Analysis of HSHA, LSHA, and LSLA Products Obtained from BBM and LBM

The grinding studies were conducted based on Bond's standard procedure to determine Bond's work index and retention time using the BBM. The effect of retention time on PSD and



Fig. 3 Laboratory ball mill

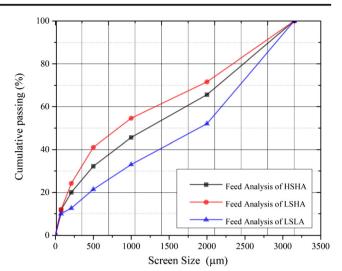


Fig. 4 Particle size analysis of HSHA, LSHA, and LSLA feed samples

the liberation of hematite from the iron ore for all the samples were analyzed.

The grinding studies in the LBM for all the iron ore samples were carried out based on the BBM total retention time taken for each representative sample obtaining 80% passing of the desired particle size fraction of 150 μ m. This study was conducted with an acceptable range of hematite liberation, and the results are analyzed and discussed in the following sections.

3.2.1 Effect of Retention Time on Passing Percentage of P_{80} Particle Size in HSHA, LSHA, and LSLA

In this section, the influence of milling time condition on the P_{80} passing percentage of HSHA, LSHA, and LSLA products produced during BBM and LBM was investigated. In the present work, one cumulative weight product passing size of 80% was specified to examine the fineness of the ground PSD of the product for different grinding conditions. The comparison of PSD of a ground product of HSHA, LSHA, and LSLA with varying grinding times of BBM and LBM is shown in Figs. 7, 8, and 9, respectively.

From Table 3, the retention time taken for HSHA, LSHA, and LSLA from BBM was 16 min, 13 min, and 12 min. For HSHA, LSHA, and LSLA, the respective BWI was 12.8 kWh/t, 10.2 kWh/t, and 8.5 kWh/t and the P_{80} passing percentage was 72 µm, 60 µm, and 48 µm. But the desired passing percentage of 150 µm for a confined retention time was not achieved in the case of BBM. Hence, the BBM grinding behavior of HSHA, LSHA, and LSLA was used in the LBM by considering retention times of 16 min, 13 min, and 12 min, respectively. By trial and error method, from Table 4, the grinding time of 14 min, 12 min, and 10 min was considered for HSHA, and the P_{80} passing percentage was 96 µm, 130 µm, and 168 µm respectively. Whereas, in the case of LSHA, with the grinding time of 11 min, 9 min, and 7 min, the P₈₀ passing percentage was

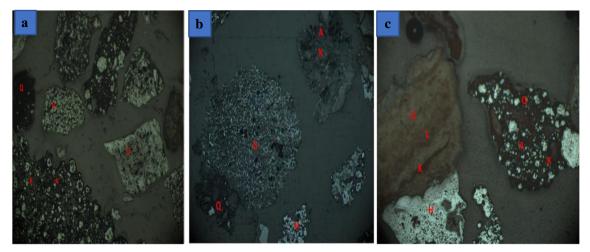


Fig. 5 Optical microscope photos for feed samples of a HSHA, b LSHA, and c LSLA

 $87 \mu m$, $119 \mu m$, and $152 \mu m$, respectively. Similarly, in the case of LSLA, with the grinding time of 10 min, 8 min, and 6 min, the P_{80} passing percentage was 75 μm , 100 μm , and 140 μm , respectively.

When compared with mineralogical and grinding parameters, it can be found that the higher the weight percentage of silica and alumina (SiO₂ is > 4.5% and Al₂O₃ > 3.5%), the higher is the P_{80} passing size of the grinding product (and therefore, the harder it is to grind). Also, the lower the weight percentage of the silica and alumina (SiO₂ is < 4.5% and Al₂O₃ < 3.5%), the lower is the P₈₀ passing size of the grinding product. This indicates that the presence of alumina and silica in the iron ore affects the grinding parameters of the ore. It is also clear that to obtain the desired percentage of P_{80} passing particle size in HSHA takes high grinding time compared with LSHA and LSLA, since the percentage of alumina and silica in HSHA is higher compared with that in LSHA and LSLA.

In comparison, the total retention time taken by each ore in the BBM is higher than the required grinding time of the ore to produce the desired PSD. The desired P_{80} is obtained after reducing 6 min from the retention time taken by each ore in the BBM. This method of controlling the retention time of the ore may save energy consumption by the mills. Finally, the optimum desired P_{80}

passing (150 μ m) percentage for HSHA, LSHA, and LSLA was 168 μ m, 152 μ m, and 140 μ m, respectively, and is shown in Figs. 7, 8, and 9, respectively.

3.2.2 Effect of Retention Time on the Degree of Hematite Liberation in HSHA, LSHA, and LSLA

Figures 10a, 11a, and 12a present the optical microscope images of the liberated hematite of HSHA (retention time of 16 min), LSHA (retention time of 13 min), and LSLA (retention time of 12 min) obtained in the BBM. From Fig. 10a, hematite liberation is higher compared with LSHA and LSLA, as shown in Figs. 11a and 12a. This is because most of the hematite particles are in a liberated state in the feed samples and most of the quartz are present in the bulk phase, which can be liberated easily from the locked hematite as shown in Figs. 5c and 6c. But in the case of HSHA and LSHA, the hematite particles were locked in quartz as finer tubular structures in feed samples and required intensive grinding to be liberated as shown in Figs. 5a, b 6a, b. Hence, the liberation of hematite in the LSLA product sample is higher than that in the HSHA and LSHA product samples.

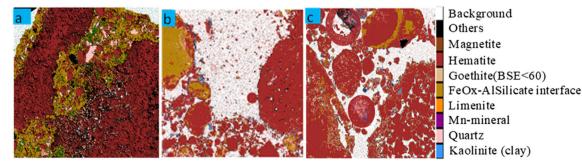


Fig. 6 QEMSCAN photos for feed samples of a HSHA, b LSHA, and c LSLA

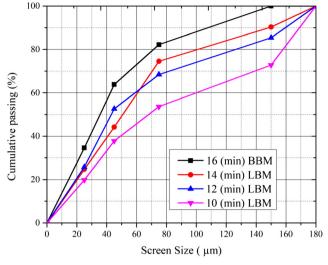


Fig. 7 Particle size analysis for HSHA product sample

The optical microscope analysis suggested that for HSHA, LSHA, and LSLA, the hematite liberation was 85%, 87%, and 93%, respectively, as shown in Table 3. However, the liberation of hematite in all the cases was well within the acceptable range (> 75%) and the P_{80} passing of all the three samples was very fine (72 µm, 60 µm, and 48 µm). The grinding results indicated that the desired P_{80} passing of 150-µm particles was not achieved for all the three types of the iron ore samples. Hence, all the three iron ore samples were further ground in the LBM based on the BBM retention time.

Figures 10b, 11b, and 12b indicate the optical microscope images of the hematite liberation of 82% for HSHA at 14 min, 84% for LSHA at 11 min, and 90% for LSLA at 10 min, respectively, using the LBM. The hematite liberation in all the cases was well within the acceptable range (hematite liberation > 75%). The P_{80} passing for all three iron ore samples was 96 µm at 14 min, 87 µm at 11 min, and 75 µm at 10 min.

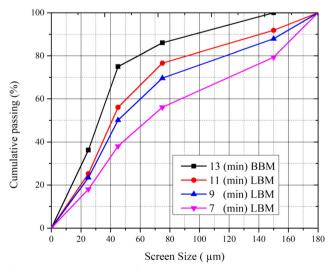


Fig. 8 Particle size analysis for LSHA product sample

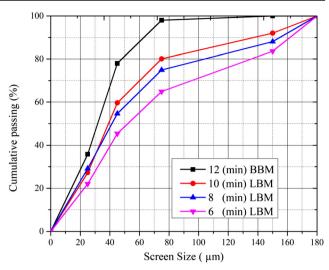


Fig. 9 Particle size analysis for LSLA product sample

Hence, the retention time of the LBM was further reduced to obtain the desirable P_{80} passing of 150-µm particles.

Figures 10c, 11c, and 12c indicate the optical microscope images of the hematite liberation of 79% for HSHA at 12 min, 81.5% for LSHA at 9 min, and 87% for LSLA at 8 min, respectively, using the LBM. The hematite liberation in all the cases was well within the acceptable range (hematite liberation > 75%). The P_{80} passing for all the three iron ore samples was 130 µm at 12 min, 119 µm at 9 min, and 100 µm at 8 min. Hence, the retention time of the LBM was further reduced to obtain the desirable P_{80} passing of 150-µm particles.

Figures 10d, 11d, and 12d indicate the optical microscope images of the hematite liberation of 78% for HSHA at 10 min, 80% for LSHA at 7 min, and 85% for LSLA at 6 min, respectively, using the LBM. The hematite liberation in all the cases was well within the acceptable range (hematite liberation > 75%). The P_{80} passing for all three iron ore samples was within the desired P_{80} passing of 150-µm particles.

On the other hand, Table 4 shows the influence of varying the grinding time on hematite liberation for HSHA, LSHA, and LSLA when ground in the LBM. The percentage of hematite liberated in all the three samples was less when ground for shorter duration. This may be due to the insufficiency of energy transmitted from the ball to the particles to crack the boundaries between the quartz and the oxidized iron minerals during the short period of grinding leading to the generation of a large number of "complex-type" locked particles without hematite liberation [41]. Due to this, mineral liberation, during short period grinding, is also very less. Also, with increasing milling time, the cracks between the quartz and the oxidized iron boundaries increase and propagate and get fractured to liberate the hematite from the locked quartz. Hence, the hematite liberation is higher with longer grinding period.
 Table 3
 Physical specification

 analysis of HSHA, LSHA, and
 LSLA using the Bond work index

 method
 Physical specification

Sl. no.	Type of ore	F ₈₀ (μm)	P ₈₀ by BBM (μm)	BWI KWh/mt	Time for 250% circulating load (min)	Percentage of hematite liberated
1	HSHA	2500	72	12.8	16	85
2	LSHA	2400	60	10.2	13	87
3	LSLA	2700	48	8.5	12	93

<u>3 LSLA 2700 48</u> Figure 13a–d shows the PSD, percentage of hematite lib-

eration, and total grinding time taken for HSHA, LSHA, and LSLA iron ore samples using BBM and LBM. The P_{80} passing percentage for HSHA is higher compared with LSHA and LSLA. This is because the percentage of SiO₂ and Al₂O₃ is higher in the HSHA feed sample, which leads to a higher grinding time compared with LSHA and LSLA. It can be observed that with an increased grinding time, the P_{80} passing percentage for all the three samples decreases, but the hematite liberation in all the three samples increases. This indicates that the grinding time is directly proportional to hematite liberation, and it is inversely proportional to the P_{80} passing percentage.

The present work was used to find the total grinding retention time of each ore in the mill. Based on the total retention time of each ore, the optimum grinding time for each ore was identified to obtain the desired P_{80} passing particle size with acceptable hematite liberation. The results obtained after considering the standard reference retention time to the LBM were improved with respect to the desired P_{80} passing percentage of 150 µm and hematite liberation. Finally, the optimum grinding time required to achieve the desired P_{80} passing percentage of 150 µm with acceptable hematite liberation percentage (75%) for HSHA, LSHA, and LSLA was 10 min, 7 min, and 6 min, respectively. The new method followed in the present work to obtain the desired P_{80} passing percentage and hematite liberation from different types of iron ore can be implemented in a pellet plant to produce desire products for pellet feed making.

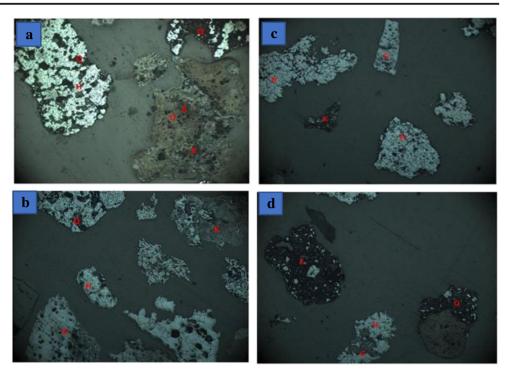
4 Conclusions

Three different samples of iron ore such as HSHA, LSHA, and LSLA were considered for the grinding studies. The characterization studies for the three iron ore samples were carried out using the optical microscopy and QEMSCAN after each stage of the grinding. The liberation studies based on the P_{80} passing percentage were discussed. BBM and LBM were used to perform the grinding. The BBM was used to calculate the total retention time taken for each ore in the mill. The estimated retention time of the iron ore in the mill was used as a standard grinding reference time to the LBM. The results obtained after considering the standard reference retention time to the LBM were improved with respect to the desired P_{80} passing percentage of 150 µm and hematite liberation. The optimum desired P_{80} passing (150 µm) percentage for HSHA, LSHA, and LSLA was 168 µm at 10 min, 152 µm at 7 min, and 140 µm at 6 min, respectively. The total retention time taken by each ore in the BBM was higher than the required grinding time of the ore to produce the desired PSD. The desired P_{80} was obtained in LBM after reducing 6 min from the total retention time taken by each ore in the BBM. By knowing the retention time of each ore, the grinding time for the desired P_{80} can be set, which will ultimately help to reduce the energy consumption by the mills. The new method

Sl. no.	Type of ore	F ₈₀ (μm)	P_{80} by LBM (μ m)	Reduced grinding time in LBM (min)	Percentage of hematite liberated
1	HSHA	2500	96	14	82
			130	12	79
			168	10	78
2	LSHA	2400	87	11	84
			119	9	81.5
			152	7	80
3	LSLA	2700	75	10	90
			100	8	87
			140	6	85

Table 4Physical specificationanalysis of HSHA, LSHA, andLSLA using LBM

Fig. 10 a Optical microscopy of HSHA sink sample of size – 150 μm grounded for 16 min in BBM. **b–d** Optical microscopy of HSHA sink sample of size – 150 μm grounded for 14, 12, and 10 min in LBM



followed in the present work to obtain the desired P_{80} passing percentage and hematite liberation from different types of iron

ore can be implemented in pellet plants to produce the desire products for pellet feed making.

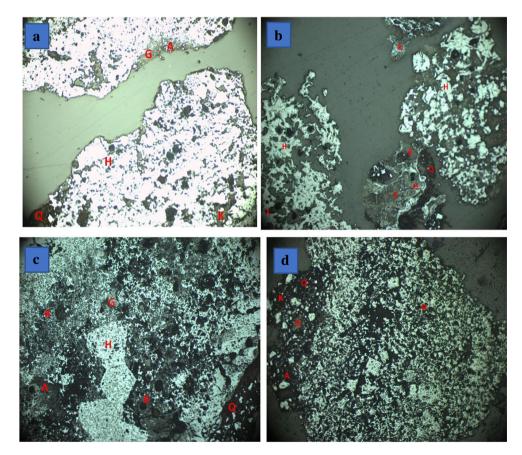
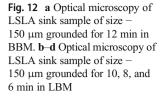
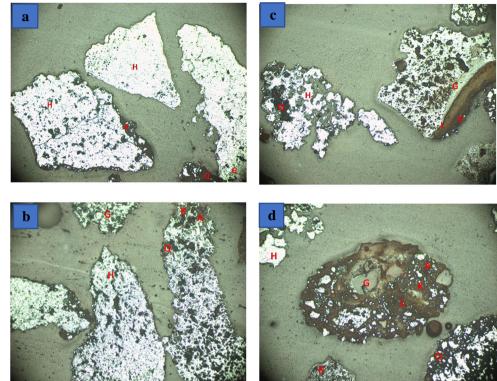


Fig. 11 a Optical microscopy of LSHA sink sample of size – 150 µm grounded for 13 min in BBM. **b–d** Optical microscopy of LSHA sink sample of size – 150 µm grounded for 11, 9, and 7 min in LBM







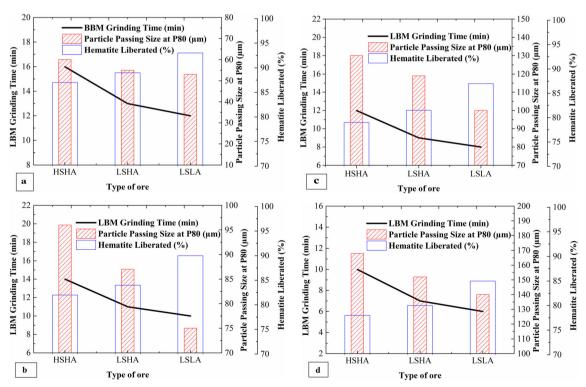


Fig. 13 a PSD, percentage of hematite liberation and total grinding time taken for HSHA, LSHA, and LSLA iron ore samples in BBM. **b**–**d** PSD, percentage of hematite liberation and total grinding time taken for HSHA, LSHA, and LSLA iron ore samples ground in LBM

Acknowledgments The present research study is carried out in collaboration between NITK, Surathkal, and JSW Steels, Ballari. The authors are thankful to the management of JSW Steels, Ballari, for their support during the course of this research work. The authors would also like to thank the management of the Partial financial support from Hutti Gold Mines Company Ltd. & Karnataka State Mineral Corporation Ltd. for their partial financial support for this work.

Compliance with Ethical Standards

Conflict of Interest The authors declare that they have no conflict of interest.

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